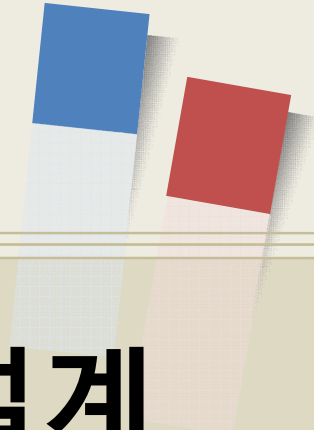


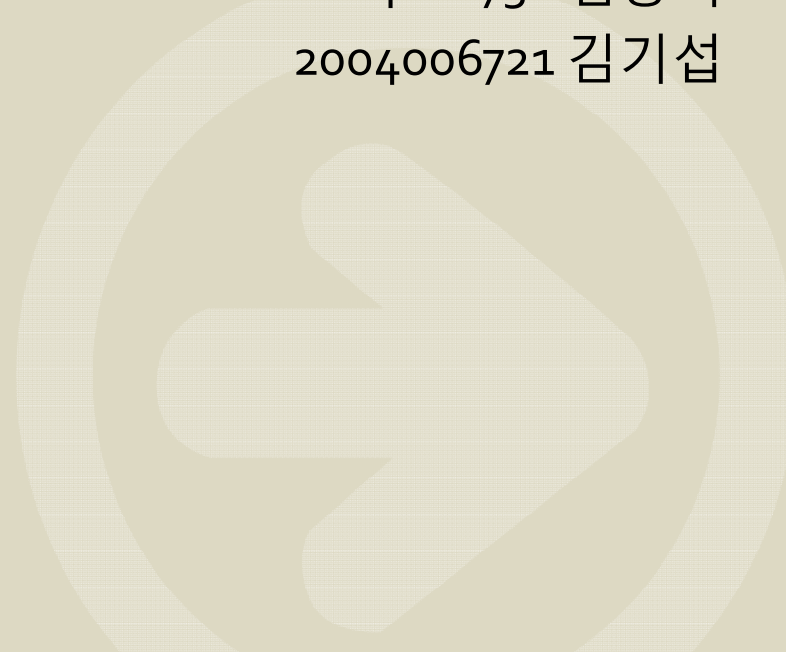


무소음 환경을 위한 Fin 설계

Kinnovation

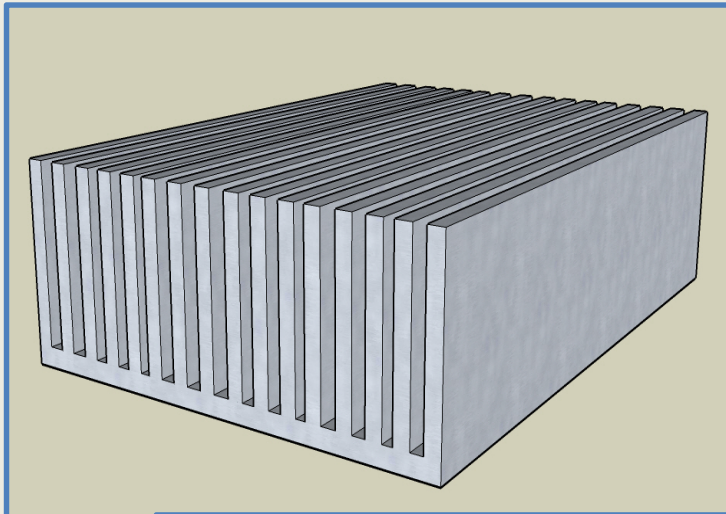
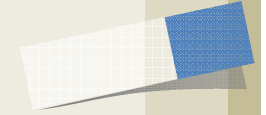
2004006732 김동석

2004006721 김기섭





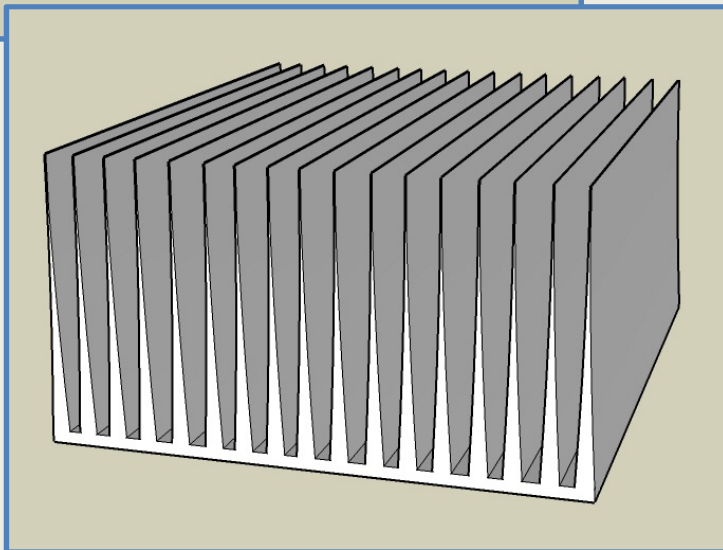
Design Object



Previous Model

2004, "Fin design" - 김민태

- Geometrical : Rectangular
- Convection : Natural Convection
Bar-Cohen, Rohsenow(1984)
- Objective of design
Maximize fin effectiveness
Minimize volume



Advanced Model

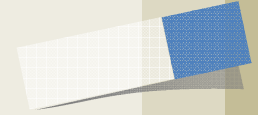
- Geometrical : Concave Parabolic
- Convection : Natural Convection
Yovanovich, Culham(1994)
- Objective of design
Minimize mass
Power consumption of CPU(65W)



Assumptions

The Murray-Gardner assumptions

- Steady state
- 1-Dimensional heat transfer
- Homogeneous and uniform characteristics of materials.
- Temp. of surrounding the fin is uniform
- Temp. at the base of the fin is uniform
- No heat source within the fin itself

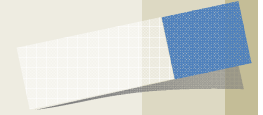


Assumptions

- Neglect radiation effect
- All heat transfer through the heat sink
- No temp. gradient between CPU and the fin base



Data and Design Variables



Properties of Air

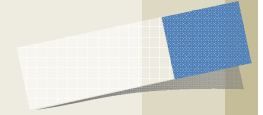
- Temp of air is 35°C
- Prandtl number, $Pr=0.7202$
- Kinematic viscosity, $\nu = 1.896 \times 10^{-5} \text{ m}^2 / \text{s}$
- Thermal expansion coefficient, $\beta = 3.0 \times 10^{-3} \text{ }^{\circ}\text{C}^{-1}$

Fin material

- Pure aluminum
- Density, $\rho = 2702 \text{ kg/m}^3$
- Thermal conductivity, $k = 237 \text{ W/m}\cdot\text{K}$



Data and Design Variables



Intermediate Variable

- H (Height of a heat sink) = $\delta_p + b$ [m]

Design Variables

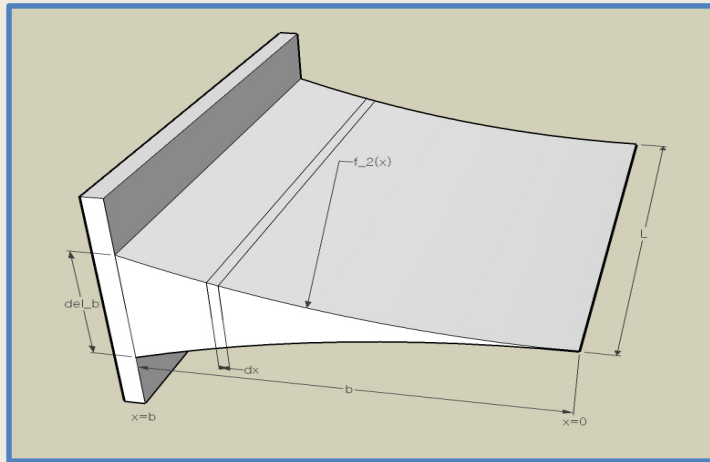
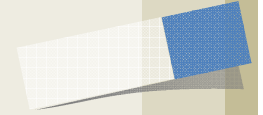
- δ_b (Thickness of a fin) [m]
- b (height of Fin) [m]
- n (Number of fins) [EA]

Parameters

- Q (Power Consumption of CPU) = 65 W
- L (Length of a Heat sink) = 0.075 m
- W (Width of a heat sink) = 0.075 m
- T_a (Temp. of air) = 35°C
- T_b (Temp. of base) = 60°C
- δ_p (Thickness of plate) = 0.001 m



Objective Function

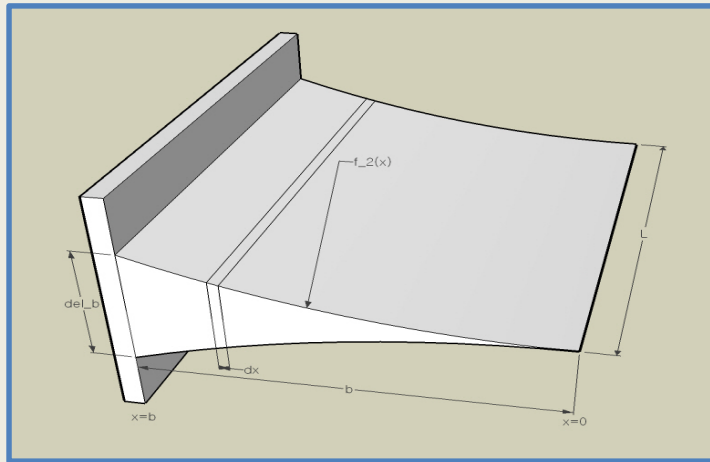
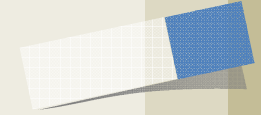


Minimize mass of the heat sink(fins).

$$f(n, \delta_b, b) = \frac{n \delta_b b^2}{3} \rho$$



Formulation - Heat transfer



- Generalized Differential Equation

$$2Lf_2(x)\frac{d^2\theta}{dx^2} + \frac{2Ldf_2(x)}{dx}\frac{d\theta}{dx} - \frac{2h}{k}\theta = 0$$

- Geometry function

$$f_2(x) = \frac{\delta_b}{2} \left(\frac{x}{b}\right)^2$$

- Solution of temp. distribution

$$\theta(b, h, \delta_b, x) = \theta_b \left(\frac{x}{b}\right)^\alpha, \text{ where } \alpha = -\frac{1}{2} + \frac{1}{2}(1 + 4m^2b^2)^{1/2}, \quad m = \left(\frac{2h}{k\delta_b}\right)^{1/2}$$

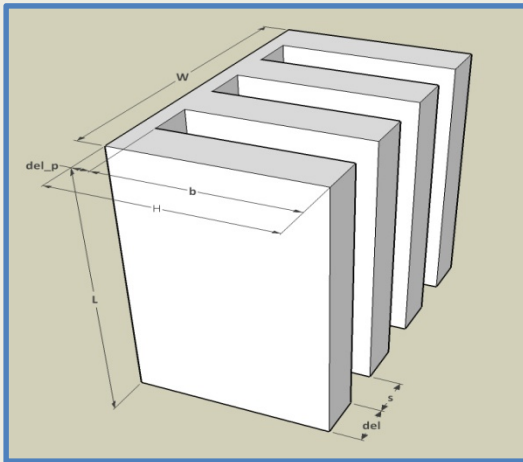
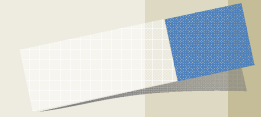
- Heat transfer through base of fin

$$\dot{Q}(b, h, \delta_b) = \frac{k\delta_b L \theta_b}{2b} (-1 + \sqrt{1 + (2mb)^2})$$



Formulation - Natural Convection

Yovanovich et al (1994)



- Nusselt numbers,
$$\text{Nu}_{\sqrt{A}} \equiv \frac{h\sqrt{A}}{k}$$
$$= \text{Nu}_{\sqrt{A}}^{\infty} + f(\text{Pr})G_{\sqrt{A}}\text{Ra}_{\sqrt{A}}^{0.25}$$

- Diffusive limit,
$$\text{Nu}_{\sqrt{S}}^{\infty} = \frac{3.192 + 1.868(H/L)^{0.76}}{\sqrt{1 + 1.189(H/L)}}$$

- Universal Prandtl number,
$$f(\text{Pr}) = \frac{0.67}{[1 + (0.5/\text{Pr})^{9/16}]^{4/9}}$$

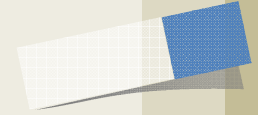
- Body gravity function

$$G_{\sqrt{S}} = 1.0904 \left[\frac{L\Lambda^2}{(n\delta_b b + \delta_b W + L\Lambda)^{3/2}} \right]^{1/4}, \text{ where } \Lambda = nb + \delta_p + W$$

- Rayleigh numbers,
$$\text{Ra}_{\sqrt{A}} \equiv \frac{g\beta\text{Pr}\Delta T(\sqrt{A})^3}{\nu^2}$$



Constraints



g1. Heat transfer

$$\dot{Q} - \dot{Q}_{total} = 65 - \left[n \times \frac{k\delta_b L \theta_b}{2b} \left(-1 + \sqrt{1 + (2mb)^2} \right) + (W - n\delta_b) L h \theta_b \right] = 0$$

g2. 1-Dimensional heat transfer

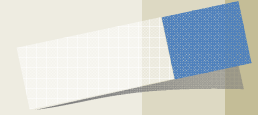
$$\frac{h\delta}{k} \leq 0.2, (\delta \leq \delta_b) \rightarrow \delta_b - \frac{0.2k}{h} \leq 0$$

g3. Fin efficiency

$$\frac{2}{1 + \sqrt{1 + (2mb)^2}} \geq 0.6 \rightarrow \frac{b^2 h}{0.96k} - \delta_b \leq 0$$



Constraints



g4. Laminar flow

$$Ra_{\sqrt{A}} - 10^9 \leq 0$$

g5. Geometry

n : natural number

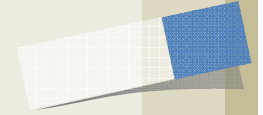
$$-\delta_b \leq 0 \quad 0.001 - \delta_b \leq 0$$

$$-b \leq 0 \quad b - 0.1 \leq 0$$

$$n\delta_b - W \leq 0$$



Graphical Solution



Design Variables

- n : number of fins
- δ_b : thickness of fin base

Fixed Variables

- b : fin height = 0.075 m

Constraints

g1. Heat transfer

$$\dot{Q} - \dot{Q}_{total} = 65 - \left[n \times \frac{k\delta_b L\theta_b}{2b} \left(-1 + \sqrt{1 + (2mb)^2} \right) + (W - n\delta_b) Lh\theta_b \right] = 0$$

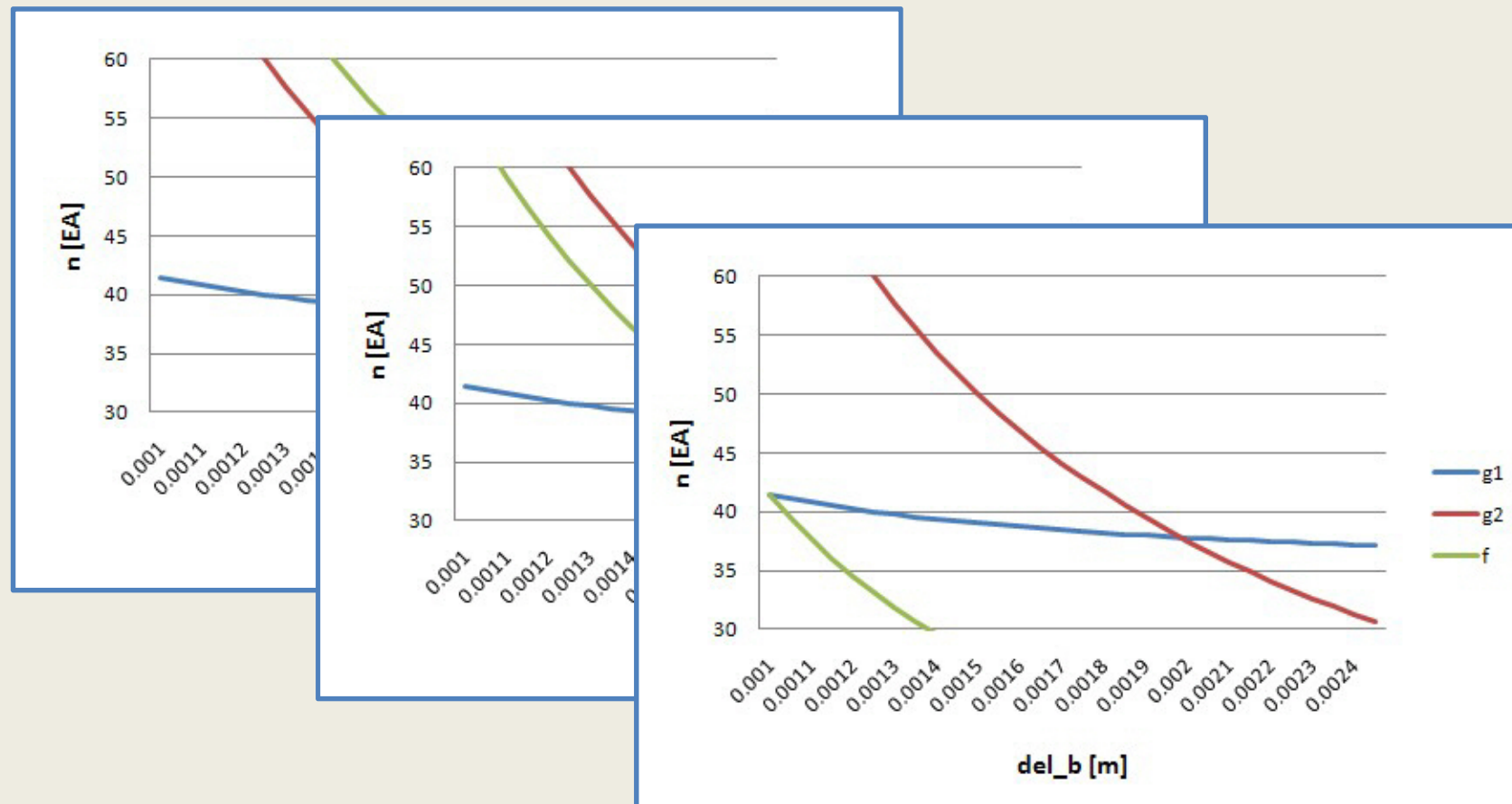
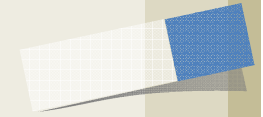
g5. Geometry

$$-\delta_b \leq 0 \quad 0.001 - \delta_b \leq 0 \quad 1 - n \leq 0 \quad n\delta_b - W \leq 0$$

n : natural number

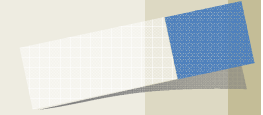


Graphical Solution

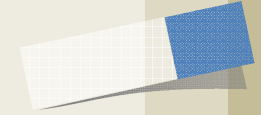




Graphical Solution



Properties			Temperature			Solutions			
k	237	W/m·°C	Base Temp.	60	°C		Initial value	Solver	
h	7	W/m²·°C	Air Temp.	35	°C	Thickness	0.001	0.0010646	m
Density	2702	kg/m³				Number of fins	41.45078	41	EA
Geometry			Input			Mass	0.21	0.2211407	kg
Width	0.075	m	CPU power	65	W	Volume	7.772E-05	8.184E-05	m³
Length	0.075	m				g1	0.0496669	2.329E-07	=0
Height	0.075	m				g2	0.0335492	0.0313502	≥0



References

Heat transfer : A practical Approach 2nd

Yunus A. Cengel

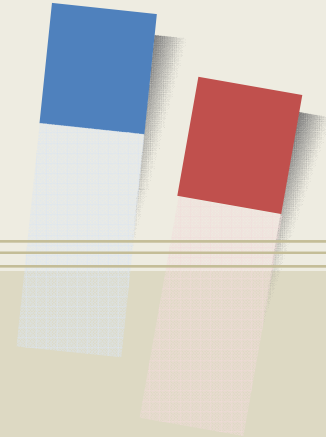
2004, McGraw-Hill

Extended Surface Heat Transfer

Allan D. Kraus, Abdul Aziz, James Welty

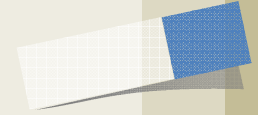
2001, Wiley Inter-Science

Questions & Answers





Appendix #1



The temp. gradient both of fin plate sides

$$\dot{Q} = k \frac{\Delta T}{L}$$

$$\Delta T = \frac{\dot{Q}L}{k} = \frac{65 \text{ W} \times 0.001 \text{ m}}{237 \text{ W/m} \cdot ^\circ\text{C}} = 0.000274^\circ\text{C}$$